Twin Screw Extrusion of Sorghum and Soya Blends: A Response Surface Analysis

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ABSTRACT

Blends of sorghum and soybean flours were processed in a co-rotating twin screw extruder to prepare expanded product. Response surface methodology (RSM) was used to study the effect of soya level (SL), feed moisture (FM), barrel temperature (BT) and screw speed (SS) on extruder system parameters and physical properties of the extrudate. Response variables were product temperature (PT), motor torque (MT), specific mechanical energy (SME), expansion ratio (ER), bulk density (BD), hardness (H), crispness (C), water absorption index (WAI), and water solubility index (WSI). Second order polynomial models were developed to determine the responses as a function of process variables. FM, BT, and SS had a significant effect on all the responses except BT on WAI, while SL considerably affected ER, BD, H, C, and WAI. All the models were found to be statistically significant ($R^2 > 0.85$; insignificant lack of fit). Sorghum-soya extruded product was found to be feasible and the optimum values of processing variables were: SL: 14 per cent; FM: 14 per cent wb; BT: 129°C; and SS: 422 rpm.

Keywords: Extrusion, RSM, SME, Sorghum, Soybean.

INTRODUCTION

Extrusion cooking - a high temperature/short time process - is an important food processing technique to develop products such as puffed snack and breakfast cereals (Brncic et al., 2010; Mahasukhonthachat et al., 2010; Santillan-Moreno et al., 2011). Extrusion has been reported to be the most effective method for enhancing protein and starch digestibility of the extrudates. Additionally, it has been used to inactivate several antinutritional compounds that limit the use of grain as a staple food (Shimelis and Rakshit, 2007; Yagc and Gogus, 2008; Alex et al., 2009).

Sorghum (*Sorghum bicolor*) is the fifth most important cereal crop in the world (Al-Rabadi et al., 2011). India is the second largest producer and consumer in the world (Charyulu et al., 2013). Sorghum is composed of carbohydrate (84.0%), protein (11%), fat (2.5%), crude fiber (2.2%), and ash (1.6%) and has an energy value of approximately 3.29 kcal g$^{-1}$ (Shobha et al., 2008). Also sorghum is a potentially important source of nutraceuticals such as antioxidant phenolics and cholesterol-lowering waxes (John et al., 2006). Although sorghum is nutritionally well comparable with other food grains, it has poor quality of protein, which leads to low solubility, deficiencies in essential amino acids (lysine and tryptophan), and interactions with tannin (Pelembe et al., 2002; Awadalkareem et al., 2008). The protein quality of sorghum can be improved by combining it with other protein-rich sources. Soybean (*Glycine max*) is an important legume, rich in quality protein (rich in lysine) and has potential to complement sorghum which is rich in sulfur containing amino acids (Pracha and Chulalak, 2000).

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Thus, the blending of sorghum and soya in appropriate proportion will make up the individual deficiencies. It has been previously reported that extruded cereal-legume products have higher protein content, high protein efficiency ratio, and improved amino acid profile (Narayan et al., 2007; Alex et al., 2009; Vargas-Solorzono et al., 2014).

From nutritional and economic point of view, fortifying sorghum with soybean flour for the production of extruded product appears to be promising. Mainly the studies involving extrusion of sorghum-based material are focused on physical and/or nutritive properties of the expanded products. The effect of extrusion on the system parameters and functional properties of sorghum-based products has not been studied in detail. Hence, the present study was conducted to investigate the effects of feed formulation and extrusion conditions on the extrusion system parameters and physical properties of a sorghum-soya extruded product using Response Surface Methodology (RSM).

RSM is a statistical mathematical method that uses quantitative data in an experimental design to determine and simultaneously solve multivariate equations to optimize processes and products. RSM is also a useful tool to minimize the numbers of trials and provide multiple regression approach to achieve optimization (Dibyakanta and Gopirajah, 2012).

MATERIALS AND METHODS

Materials

Sorghum (DSV-4 variety) and Soybean (MAUS-2 variety) grains were procured from Directorate of Sorghum Research, Hyderabad, India, and AICRP on Soybean, Bangalore, India, respectively. After thorough cleaning, both sorghum and soya grains were ground to flour in a laboratory scale hammer mill, equipped with 60-mesh IS sieve.

Extrusion Cooking

Extrusion experiments were performed on a laboratory scale co-rotating twin-screw extruder (Basic Technology Pvt. Ltd., Kolkata, India). The length to diameter ratio (L/D) was 8:1. The extruder had two barrel zones. Temperature of the first zone was maintained at 74°C throughout the experiments, whereas at the second zone (die section) was varied according to the experimental design. The circular die of 3.0 mm was used in the entire study. Blends of sorghum and soya flour were prepared as per the experimental design using a ribbon blender (GL Extrusion Systems, New Delhi, India) for 20 minutes. Simultaneously, the moisture content of the blends were also ascertained. Moisture conditioning of blends were done through moisture addition (AACC, 1983; Liu et al., 2000).

Preconditioned feed mixture was metered into the extruder by a twin-screw volumetric feeder equipped with it. The speed of the feeder screw was adjusted so as to get a feed rate of 5 kg h⁻¹ for the entire study. Extruded samples were collected in stainless steel trays for 5 minutes after the extruder system parameters (PT and MT) reached a steady-state condition. The trays were then kept in a cabinet drier (MSW-216, Marco Scientific Works, New Delhi) at 60°C for 1 hour and cooled to room temperature. The dried samples were stored in polythene bags at room temperature (25±4°C) until analyzed. All trials were conducted in 3 replications.

Experimental Design and Statistical Analysis

RSM was used to investigate the effects of SL and extrusion conditions on the process and product responses. The independent variables considered for this study were: Soya Level (SL): 10-30%; Feed Moisture (FM): 12-20% wb; Barrel Temperature (BT): 110-150°C, and Screw Speed (SS): 250-450 rpm. The levels of each variable were established according to the literature and preliminary
trials. Dependent variables were the product temperature (PT), motor torque (MT), specific mechanical energy (SME), expansion ratio (ER), bulk density (BD), hardness (H), crispness (C), water absorption index (WAI), and water solubility index (WSI). Central composite rotatable design was used to design the experiment. The design required 30 experimental runs (6 central, 8 axial, and 16 factorial points). Regression analysis was done to assess the effects of SL, FM, BT and SS on dependent variables. The experimental data obtained were analyzed after fitting them into a second order polynomial model

\[ y_i = b_0 + \sum_{i=1}^{4} b_i X_i + \sum_{i=1}^{4} \sum_{j=1}^{4} b_{ij} X_i X_j \]

Where, \(X_i, X_j, X_{ij}\), and \(X_{Xj}\) are linear, quadratic, and interaction effect of the input variables which influence the response \(y\), respectively, and \(b_0, b_i, b_{ij}\) are the regression coefficients to be determined. RSM was applied using a commercial statistical package, Design-Expert version 8.0.7 (Stat-Ease Inc., Minneapolis, USA), for the generation of response surface plots. The adequacy of the models was determined using model analysis, lack-of-fit test and coefficient of determination (R²) analysis.

### Determination of Responses

#### System Responses

PT and MT as displayed on the extruder control panel were recorded twice, in the beginning and the end of product collection. SME \((\text{Wh kg}^{-1})\) was calculated from the rated screw speed (1445 rpm), motor power rating (5.5 kW), actual screw speed, percentage MT, and mass flow rate (5 kg h\(^{-1}\)) using the following formula (Normell et al., 2009):

\[
\text{SME} = \frac{\text{actual screw speed, rpm}}{\text{rated screw speed, rpm}} \times \frac{\% \text{motor torque}}{100} \times \frac{\text{motor power rating, kW}}{\text{mass flow rate, kg h}^{-1}} \times 1000
\]

### Expansion Ratio

To determine the ER, the cross-sectional diameter of the extrudates was determined with a digital Vernier caliper. The ratio of diameter of extrudate and the diameter of die was used to express the expansion of extrudate (Pansawat et al., 2008). The ER values were obtained from 10 random samples for each extrusion condition.

### Bulk Density

BD was calculated by measuring the actual dimensions of the extrudates. After weighing the extrudate, its diameter and length were measured using a digital Vernier caliper. The BD was estimated using the following formula, assuming a cylindrical shape of the extrudate (Sibel and Fahrettin, 2008).

\[
\text{Bulk density} = \frac{4m}{\pi d^2 l}
\]

Where, \(m\) is mass of the extrudate (g), \(d\) is diameter (cm), and \(l\) is the length (cm). Ten pieces of extrudates were randomly selected and their average taken.

### Texture

Force-deformation data for each extrudate were obtained using a Texture Analyzer (TA HDi, Stable Micro Systems Ltd., UK) fitted with 50 kg load cell and 2 mm diameter test probe. Tests were conducted in compression mode and the probe was allowed to penetrate the product a depth of 3 mm. The peak force in N was taken as a measure of H (Meng et al., 2010) whereas C was measured in terms of number of positive peaks (Subir et al., 2011). The test settings included pre-test speed of 5 mm s\(^{-1}\), test speed of 2 mm s\(^{-1}\), and post-test
speed of 5 mm s\(^{-1}\). Force-deformation curve was recorded and analyzed using an inbuilt software program. Ten randomly collected samples were measured for each extrusion condition and the mean of the observations was recorded.

**Water Absorption and Solubility Indices**

\(WAI\) and \(WSI\) of extrudates were determined by a method used by Sibel and Fahrettin (2008). The extrudate samples were ground and sieved through 500 \(\mu\)m sieve. A 0.5 grams of sample (extrudate flour) was weighed into a centrifuge tube along with 10 mL of distilled water at 25°C and thoroughly mixed to produce a smooth dispersion. Samples were allowed to settle for 30 minutes with intermittent shaking for every 5 minutes, then, centrifuged (SIGMA 3-18K, SciQuip, UK) at 1,800\(\times\)g for 15 minutes. The supernatant was decanted into a tared aluminum pan and dried to constant weight at 105°C. The weight of the gel remaining in the centrifuge tube was noted. The results were expressed as the average of two measurements.

\[
WAI, \frac{g}{g} = \frac{\text{Weight gain by gel}}{\text{Dry weight of extrudate}}
\]

\[
WSI, \% = \frac{\text{Weight of dry solids in supernatant}}{\text{Dry weight of extrudate}} \times 100
\]

**Optimization**

Optimum values of the processing variables were obtained with the help of the numerical optimization technique of the Design-Expert software (ver. 8.0.7). The software necessitates assigning goals to the processing variables and the responses. The software was used to generate optimum processing conditions and also to predict the corresponding response.

**RESULTS AND DISCUSSION**

Effects of extrusion conditions on the process and product responses are shown in Table 1. The estimated regression coefficients of the second order polynomial models for the various responses and their statistical validity defining values are reported in Table 2. The regression models for all the responses were highly significant (P< 0.01), with a high coefficient of determination (\(R^2 > 0.86\)). Furthermore, F-values reflected that all the models were significant. Coefficient of variation being lower than 10 per cent suggests the reasonable accuracy of the experiments and reproducibility of the models. Non significant lack-of-fit (P< 0.05) indicate that the models correlated well with the measured data.

**Process Response**

**Product Temperature (PT)**

The predicted response model (Table 2) indicated that the linear effects of \(FM\), \(BT\), and \(SS\), and the quadratic effects of \(BT\) and \(SS\) were the determining factors for \(PT\). Among the four variables, \(BT\) had a prominent effect on \(PT\). The response surface plots [Figure 1, (a and b)] showed that increase in \(BT\) and \(SS\) led to an increased \(PT\), whereas increase in \(FM\) lowered the \(PT\). The interaction term \(BT-SS\) had a significant (P< 0.1) negative effect. \(PT\) values ranged between 116 and 156°C (Table 1).

\(PT\) plays an important role in changing the rheological properties of the extruded melts, which in turn affects the degree of expansion. The recorded temperatures were higher than the set \(BT\) (110-150°C), which could be due to the generation of heat through dissipation of mechanical energy during extrusion. Frame (1994) reported that the heat was generated during extrusion by inter-particulate friction, and friction between the material, the screw elements, and the barrel. Similar results were observed by Pansawat et al. (2008) and Meng et al. (2010). The significant (P< 0.05) negative effect of \(FM\) could be due to the reason that
## Table 1. Effects of extrusion conditions on process and product responses.

<table>
<thead>
<tr>
<th>Extrusion condition</th>
<th>Process responses</th>
<th>Product responses</th>
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<tbody>
<tr>
<td></td>
<td>PT (°C)</td>
<td>MT (%)</td>
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<tr>
<td>SL (%)</td>
<td>FM (%)</td>
<td>BT (°C)</td>
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<tr>
<td>15</td>
<td>14</td>
<td>120</td>
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<tr>
<td>20</td>
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<td>130</td>
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</tbody>
</table>

* SL: Soya Level; FM: Feed Moisture; BT: Barrel Temperature; SS: Screw Speed; PT: Product Temperature; MT: Motor Torque; SME: Specific Mechanical Energy; ER: Expansion Ratio; BD: Bulk Density; WA1: Water Absorption Index; WSI: Water Solubility Index. Data are mean values and means from 2, 10 and 3 measurements, respectively.
Table 2. ANOVA and regression coefficients of the second order polynomial models of the various responses.

<table>
<thead>
<tr>
<th>Parameters</th>
<th>Regression coefficients</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>PT (^c)</td>
</tr>
<tr>
<td>Intercept</td>
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</tr>
<tr>
<td>X(_1) (^d)</td>
<td>-0.125</td>
</tr>
<tr>
<td>X(_2) (^b)</td>
<td>-1.54**</td>
</tr>
<tr>
<td>X(_3) (^c)</td>
<td>8.29***</td>
</tr>
<tr>
<td>X(_4) (^d)</td>
<td>1.54**</td>
</tr>
<tr>
<td>X(_1)X(_1)</td>
<td>0.06</td>
</tr>
<tr>
<td>X(_2)X(_2)</td>
<td>-0.06</td>
</tr>
<tr>
<td>X(_3)X(_3)</td>
<td>0.31</td>
</tr>
<tr>
<td>X(_4)X(_4)</td>
<td>0.56</td>
</tr>
<tr>
<td>X(_1)X(_2)</td>
<td>-0.56</td>
</tr>
<tr>
<td>X(_1)X(_3)</td>
<td>-1.19*</td>
</tr>
<tr>
<td>X(_1)X(_4)</td>
<td>-0.05</td>
</tr>
<tr>
<td>X(_2)X(_2)</td>
<td>-0.55</td>
</tr>
<tr>
<td>X(_3)X(_3)</td>
<td>-1.17**</td>
</tr>
<tr>
<td>X(_4)X(_4)</td>
<td>-0.93*</td>
</tr>
<tr>
<td>ANOVA</td>
<td>R(^2)</td>
</tr>
<tr>
<td>Model F-value</td>
<td>18.6***</td>
</tr>
<tr>
<td>Lack of fit (p value)</td>
<td>0.242</td>
</tr>
<tr>
<td>C.V. (^%)</td>
<td>1.95</td>
</tr>
</tbody>
</table>

\(^a\) Coded soya level; \(^b\) Coded feed moisture; \(^c\) Coded barrel temperature; \(^d\) Coded screw speed; \(^e\) Product Temperature; \(^f\) Motor Torque; \(^g\) Specific Mechanical Energy; \(^h\) Expansion Ratio; \(^i\) Bulk Density; \(^k\) Water Absorption Index; \(^l\) Water Solubility Index. * Significant at 10% (P<0.1); ** Significant at 5% (P<0.05); *** Significant at 1% (P<0.01).
the water acts as a plasticizer in the extruder; therefore any increase in FM reduces the melt viscosity and dissipation of mechanical energy (Ilo et al., 1996). SS had a significant (P< 0.05) positive effect on PT. This may be attributed to dependence of shear or mechanical energy on SS (Meng et al., 2010). A higher screw speed generates a greater amount of mechanical energy or frictional heat and, hence, increases PT. Furthermore, mean residence time also influence heat generation and mass temperature. Decrease in PT at very high SS (Figure 1-b) could be due to reduced mean residence time at high SS.

Motor Torque and Specific Mechanical Energy

MT provides information about the amount of energy absorbed by the material, while SME is the mechanical energy input per unit mass of the extrudate (Altan et al., 2008; Pansawat et al., 2008). The regression analysis results (Table 2) indicated that the liner terms of FM and BT had a significant (P< 0.01) negative effect on MT and SME, while SS had a significant negative effect on MT and positive effect on SME. The effect of SL was mainly quadratic (P< 0.01). However, interaction between the independent variables had no significant effect. The measured MT values ranged from 30.25% to 50.65 per cent and the calculated SME from 81.33 to 146.53 Wh kg⁻¹ (Table 1).

Any variable affecting the viscosity of the food melts in the extruder would correspondingly effect MT and SME (Akdogan, 1996). Elevating the BT or FM caused a decline in the melt viscosity, consequently, decreasing the SME (Figure 2) and MT. The degree of fill in the extruder barrel manipulates the torque requirement (Jin et al., 1994; Meng et al., 2010). At a constant feed rate, an increase in SS decreased the length of filled flights resulting in reduced load on the screw shaft thereby lowering the MT (Figure 3). Although a decrease in SME was expected as melt viscosity would decrease with increasing SS, the present study indicates that the effect of SS dominates the effect of melt viscosity. This could be attributed to the increased shear rate with increase in SS, the present study indicates that the effect of SS dominates the effect of melt viscosity. This could be attributed to the increased shear rate with increase in SS, and is a well-documented observation in various studies (Akdogan, 1996; Altan et al., 2008; Normell et al., 2009). The significant effect (P< 0.01) of quadratic term of SL on MT and SME implies a considerable increase in these two responses after a certain level of soya. This is also reflected on the surface plot (Figure 3) with a curved surface. This result revealed that the viscosity effect, at lower levels of soya, was dominated by the
binding action of high protein content in the feed blend at high SL.

**Product Response**

**Expansion Ratio and Bulk Density**

$ER$ and $BD$ describe the degree of expansion undergone by the melt as it exits the extruder, while $ER$ considers expansion only in the direction perpendicular to the extrudate flow, $BD$ considers expansion in all directions (Altan et al., 2008). The regression results (Table 2) indicated that all the investigated variables had a significant ($P < 0.01$) effect on $ER$ and $BD$. $ER$ was significantly affected by the quadratic term of $SL$, while $BD$ by $BT$ and $SS$. Interaction terms of $SL$-$BT$ and $FM$-$SS$ were found to be significant on $BD$. The $ER$ of extrudates varied between 2.357 and 3.475, while $BD$ varied between 103 and 377 kg m$^{-3}$ (Table 1).

The significant effect of $FM$ on $ER$ and $BD$ could be due to either changed molecular structure of amyllopectin, which reduces the melt elasticity (Ilo et al., 1996), or extrusion cooking is not enough to cause vaporization of moisture resulting in reduced expansion and increased density (Asare et al., 2012). Increase in $BT$ increased $ER$ while reducing $BD$, probably due to enhanced gelatinization of starch, which increases the volume of extrudates (Case et al., 1992). In addition, high temperature provides higher potential energy for flash-off of super-heated water from extrudates with increased linear velocity at the die favoring expansion (Koksel et al., 2004). At low moisture levels, $ER$ increased with $BT$ before it reached a critical level after which it declined (Figure 4). This may be caused by dextrinization of starch and weakening of structure (Dogan and Karwe, 2003). $ER$ decreased and $BD$ increased with increase in $SL$. This could be attributed to the dilution effect of soya on starch, which may affect the extent of starch gelatinization and, thus, the rheological properties of the melted material (Sibel and Fahrettin, 2008). The significant ($P < 0.01$) negative effect of $SS$ on $BD$ (Figure 5) and $ER$ could be attributed to the structural breakdown under increased shear environment. Increasing $SS$ tends to increase the shearing effect, this causes protein and starch molecules to be stretched farther apart, weakening bonds and resulting in a puffer product (Filli et al., 2012). The effect of $FM$ and $SS$ were found to be dependent on each other (Table 3). Similar results have been reported earlier for different types of the extruded products.

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**Figure 2.** Response surface plot for $SME$ as a function of $FM$ and $BT$ while other variables are at center point.

**Figure 3.** Response surface plot for $MT$ as a function of $SL$ and $SS$ while other variables are at center point.
Hardness and Crispness

Hardness (H) of the expanded extrudates is a sensory perception of the human being and is associated with expansion and cell structure of the product, while crispness (C) is typically a textural attribute (Meng et al., 2010). H and C were significantly (P< 0.01) affected by the linear terms of all predictor variables. Increasing SL and FM and decreasing BT and SS significantly increased H, while reducing C (Table 2). The variables also had a significant quadratic effect (P< 0.01) on H and C, except SL on C. Comparing the regression coefficients, it was observed that the FM had a maximum influence on H and C, followed by the BT, SS, and SL. Hardness of the extrudates varied between 39.4 and 295.2 N, while C, as the number of positive peaks, ranged between 16.9 and 29.4 (Table 1).

Chang et al. (1998) suggested that the degree of expansion affects density, fragility, and softness of the extruded products. H increased (Figure 6) and C decreased with increase in SL and FM. This is in agreement with the degree of cooking, as indicated by ER in this study. Increasing SL and FM decreased the degree of starch gelatinization and, as a result, pore wall became thicker and hard and heavy product was obtained (Adrian et al., 2008). This result is in consistent with those of Liu et al. (2000), Li et al. (2005) and Normell et al. (2009). The significant (P< 0.01) negative effect of BT on H is in line with the BD, where an increase in BD was observed (Table 2). Ding et al. (2005) reported that the increase in BT would decrease the melt viscosity, but increases the vapor pressure of water which favors the bubble growth and, consequently, expansion. Thus increase in BT resulted in a soft and crispy product. Similar results were reported by Altan et al. (2008). Increase in SS increased C (Figure 7) while reducing H. This may be attributed to the relative increase in the amount of mechanical energy delivered to the extruded material at higher SS. In this study, this could be explained by the significant positive influence of SS on SME (Table 2). This increased mechanical energy delivered to the material at higher SS might have enhanced starch conversion, leading to crispier product (Meng et al., 2010). The interaction between FM and SS was significant (P< 0.01), which means that the higher values of H at high levels of FM were dependent on SS. Similar effect of SS has been observed in corn (Altan et al., 2008), barley (Liu et al., 2000) and chickpea (Meng et al., 2010) based extrudates.
Water Absorption and Water Solubility Indices

WAI and WSI are two important measures related to the degree of starch conversion or damage as a result of extrusion processing (Normell et al., 2009). WAI measures the amount of water absorbed by starch and can be used as an index of starch gelatinization, while WSI indicates degradation of starch molecules (Sibel and Fahrettin, 2008). The statistical analysis demonstrated that linear terms of $SL$, $FM$ and $SS$ had a significant effect on the WAI and WSI, with the exception of $SL$ on WSI. The interaction between the variables had no significant effect, except $FM$ and $BT$ interaction on WAI ($P < 0.1$). The quadratic terms of $FM$-$BT$ had a significant ($P < 0.05$) positive effect, respectively, on WAI and WSI. The value of WAI ranged between 3.78 and 5.35 g g$^{-1}$ dry sample, while WSI varied between 14.59 and 23.21% (Table 1).

The WAI decreased significantly ($P < 0.01$) as $SL$ increased (Figure 8), mainly because of reduction in the starch content. Relative decrease in starch content with addition of soya may affect the extent of starch gelatinization in barrel and caused reduced water absorption. Similar effects of adding non-starch components on WAI have been reported earlier for millet-legume blend (Subir et al., 2011). It is generally agreed that $FM$ exerts the greatest effect on the extrudate by promoting gelatinization (Ding et al., 2005). At high moisture content, the viscosity of the starch would be low, which allows extensive internal mixing and uniform heating that would account for enhanced starch gelatinization while diminishing starch degradation (Miranda et al., 2011). Further, low moisture conditions results in greater shear degradation of starch during extrusion (Anastase et al., 2006). Therefore, WAI increased and WSI decreased with increase in $FM$. Similar effects were reported earlier for rice based extrudates (Ding et al., 2005). The significant ($P < 0.05$) negative effect of $SS$ on WAI suggests that higher SS degraded starch into smaller fragments, which are more soluble in water. High input of thermal energy due to high residence time (at low SS) may enhance starch degradation and increase WSI (Figure 9). The effect of $SS$ on molecular degradation and gelatinization of starch is in agreement with van den Einde et al. (2004) and Normell et al. (2009). WSI is reported to be related to the presence of soluble molecules that have sometimes been
attributed to dextrinization (Anastase et al., 2006). The significant (P< 0.05) quadratic positive effect of BT on WSI could be probably due to increased dextrinization at higher BT.

**Optimization**

Optimization was carried out under the following constraints: maximize soya level, ER, SME, C, WAI, and WSI; minimize BD and H. The optimum conditions obtained for SL, FM, BT, and SS were 14 per cent, 14 per cent wb, 129°C and 422 rpm, respectively. The corresponding optimum values of ER, SME, C, WAI, WSI, BD and H were 3.319, 140 Wh kg⁻¹, 27, 4.33 g g⁻¹, 23.45 per cent, 102.2 kg m⁻³, and 42 N, respectively.

**CONCLUSIONS**

This study analyzed the effect of processing variables on the responses of extrudates manufactured from different blends of sorghum and soybean. The models were found to be statistically valid and provided adequate information regarding the behavior of the responses upon variation in the processing variables. The results showed that various levels of soybean could be incorporated into extruded sorghum based snacks depending on the desired qualities of the product. The products with high ER and C and low BD and H, which are generally good characteristics of extruded snacks, were produced at low FM, high SS, medium to high BT, and medium SL. The study confirms the feasibility of developing nutritious snack food from sorghum-soya by extrusion processing.

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**REFERENCES**


Twin Screw Extrusion of Sorghum and Soya Blends


خروجی مخلوط سورگم و سویا از دستگاه روزن ران پلاستیک: تجزیه به روش سطح واکنش

ت. و. آرون کومار، د. و. ک. سامونل، س. ک. جها، و. ج. پ. سپهایا

چکیده

برای تولید یک محصول مخلوط آرد سورگم و سویا در یک دستگاه اکسترودر با روزن ران (twin screw extruder) و همچنین درجه حرارت شکن (SS)، برای برسی اثراتی مقدار سویا (FM) و سرعت پیچ (BT)، مقدار یکی از موارد خروجی از دستگاه مزبور از تجزیه به روش سطح واکنش استفاده شد. متغیرهای واکنش (Response surface methodology) شامل: محمد نامداریان (BD)، گشتاور موتور (MT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)، انرژی مکانیکی ویژه (SME)، جرم مخصوص (Wei) در حرارت محصول (PT)